

Name:
Enrolment No:



UPES

End Semester Examination, December 2023

Course: Chemical Reaction Engineering I
Program: B. Tech Chemical Engineering
Course Code: CHCE3004

Semester: V
Time: 03 hrs.
Max. Marks: 100

Instructions: This is an OPEN BOOK, OPEN NOTES, AND OPEN RESOURCE examination. The students are allowed to carry any TEXTBOOKS, HANDWRITTEN AND PHOTOCOPIED NOTES, AND LAPTOP.

Please read all the questions carefully. Take and mention all necessary assumptions.

SECTION A (100 marks)

S. No.		Marks	CO																																										
	<p>You and your supervisor are working in an ethylene plant. Both of you feel that there is something wrong with the current process. Your supervisor gives you the kinetic data set given below and asks you to check for the kinetic equations that can be used for reactor design.</p> <p>The reaction follows the following stoichiometry</p> $2C_2H_4 + O_2 \rightarrow 2C_2H_4O$ $2A + B \rightarrow 2C$ <table border="1"><thead><tr><th>t (min)</th><th>C_A (kmol/m³)</th><th>C_B (kmol/m³)</th></tr></thead><tbody><tr><td>0*T</td><td>1*C_{ao}</td><td>1*C_{bo}</td></tr><tr><td>0.01*T</td><td>0.99*C_{ao}</td><td>0.870*C_{bo}</td></tr><tr><td>0.02*T</td><td>0.91*C_{ao}</td><td>0.740*C_{bo}</td></tr><tr><td>0.03*T</td><td>0.83*C_{ao}</td><td>0.610*C_{bo}</td></tr><tr><td>0.04*T</td><td>0.76*C_{ao}</td><td>0.480*C_{bo}</td></tr><tr><td>0.05*T</td><td>0.68*C_{ao}</td><td>0.350*C_{bo}</td></tr><tr><td>0.06*T</td><td>0.60*C_{ao}</td><td>0.220*C_{bo}</td></tr><tr><td>0.07*T</td><td>0.52*C_{ao}</td><td>0.090*C_{bo}</td></tr><tr><td>0.08*T</td><td>0.44*C_{ao}</td><td>0.083*C_{bo}</td></tr><tr><td>0.09*T</td><td>0.37*C_{ao}</td><td>0.076*C_{bo}</td></tr><tr><td>0.10*T</td><td>0.29*C_{ao}</td><td>0.068*C_{bo}</td></tr><tr><td>0.11*T</td><td>0.21*C_{ao}</td><td>0.061*C_{bo}</td></tr><tr><td>0.12*T</td><td>0.13*C_{ao}</td><td>0.054*C_{bo}</td></tr></tbody></table>	t (min)	C _A (kmol/m ³)	C _B (kmol/m ³)	0*T	1*C _{ao}	1*C _{bo}	0.01*T	0.99*C _{ao}	0.870*C _{bo}	0.02*T	0.91*C _{ao}	0.740*C _{bo}	0.03*T	0.83*C _{ao}	0.610*C _{bo}	0.04*T	0.76*C _{ao}	0.480*C _{bo}	0.05*T	0.68*C _{ao}	0.350*C _{bo}	0.06*T	0.60*C _{ao}	0.220*C _{bo}	0.07*T	0.52*C _{ao}	0.090*C _{bo}	0.08*T	0.44*C _{ao}	0.083*C _{bo}	0.09*T	0.37*C _{ao}	0.076*C _{bo}	0.10*T	0.29*C _{ao}	0.068*C _{bo}	0.11*T	0.21*C _{ao}	0.061*C _{bo}	0.12*T	0.13*C _{ao}	0.054*C _{bo}		
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	<p>Here,</p> <p>T = Last THREE digits of your SAP ID (min)</p> <p>Cao and Cbo = Last TWO digits of your ROLL NUMBER (kmol/m³)</p>																														
Q1.	What will be the rate law for the above kinetic data? Choose your methodology with justification. Mention all the necessary assumptions taken.	15	CO2																												
Q2.	Note your observations from Q1 and analyze your conclusions with detailed reasoning and assumptions.	15	CO1																												
Q3.	<p>Based on the above kinetic equations, your supervisor wishes you to choose for the best reactor arrangements from below to meet the required conversion if the molar flowrates for A and B are 10 kmol/min and 12 kmol/min respectively.</p> <p>i) One CSTR (97% conversion)</p> <p>ii) PFR (40% conversion) + PFR (30% conversion) + CSTR (27% conversion) [in series]</p> <p>iii) PFR (40% conversion) + CSTR (30% conversion) + PFR (27% conversion) [in series]</p> <p>iv) CSTR (40% conversion) + PFR (30% conversion) + PFR (27% conversion) [in series]</p> <p>Give proper justification for your choice.</p>	20	CO4																												
Q4.	<p>Your supervisor is happy with your findings and reactor design. However, you realized that the design is based on ideal conditions and the reactor that you have in the plant will have non-ideal conditions. To identify the same you did tracer RTD analysis with pulse input and received the following data</p> <table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th>t (min)</th> <th>C (g/min)</th> </tr> </thead> <tbody> <tr><td>0*T</td><td>0*Ci</td></tr> <tr><td>0.1*T</td><td>0.18*Ci</td></tr> <tr><td>0.2*T</td><td>0.98*Ci</td></tr> <tr><td>0.3*T</td><td>1.10*Ci</td></tr> <tr><td>0.4*T</td><td>1.90*Ci</td></tr> <tr><td>0.5*T</td><td>3.90*Ci</td></tr> <tr><td>0.6*T</td><td>4.00*Ci</td></tr> <tr><td>0.7*T</td><td>2.60*Ci</td></tr> <tr><td>0.8*T</td><td>1.80*Ci</td></tr> <tr><td>0.9*T</td><td>1.28*Ci</td></tr> <tr><td>1.0*T</td><td>0.44*Ci</td></tr> <tr><td>1.1*T</td><td>0.10*Ci</td></tr> <tr><td>1.2*T</td><td>0.08*Ci</td></tr> </tbody> </table> <p>Here,</p>	t (min)	C (g/min)	0*T	0*Ci	0.1*T	0.18*Ci	0.2*T	0.98*Ci	0.3*T	1.10*Ci	0.4*T	1.90*Ci	0.5*T	3.90*Ci	0.6*T	4.00*Ci	0.7*T	2.60*Ci	0.8*T	1.80*Ci	0.9*T	1.28*Ci	1.0*T	0.44*Ci	1.1*T	0.10*Ci	1.2*T	0.08*Ci		
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	a. Generate the <i>Exit age distribution curve</i> from the data you received from the experiments.	5	CO2
	b. Calculate the “ <i>moments for the curve</i> ” and the “ <i>Vessel dispersion number</i> ” for the data.	10	CO2
	c. Based on the calculations in part a) and b) note down your observations and analyze your inferences with detailed reasoning and assumptions.	15	CO1
	d. As you need to run these reactions and get the final product your supervisor is interested in knowing what conversion we achieve in the reactor. Choose your model and calculate the expected conversion for your reactor. Provide reasoning for your choice of the model. Comment on the conclusions that you derive from the above results.	20	CO4