

<b>Name:</b>	
<b>Enrolment No:</b>	

**UNIVERSITY OF PETROLEUM AND ENERGY STUDIES**  
**End Sem Examination, December 2019**

**Course: Chemical Reaction Engineering**  
**Program: B. Tech APE GAS**  
**Time: 02 hrs.**

**Semester: VII**  
**Code: CHEG331**  
**Max. Marks: 100**

**Instructions: Answer all the questions of a section at one place and in order. Write legibly.**

**SECTION A (60 Marks)**

S. No.		Mar ks	CO
Q 1	Derive an expression for the concentration of reactant in the exit stream from a series of mixed reactors of different sizes. Assume that the reaction follows first order kinetics and the holding time in the $i_{th}$ reactor is $\tau_i$ .	<b>10</b>	<b>CO1</b>
Q 2	The elementary liquid phase reaction $A+B \rightarrow R+S$ is carried out in a plug flow reactor. For equimolar amounts of A and B ( $C_{A0} = C_{B0} = 0.9$ mol/lit), 94% conversion is achieved in it. If a CSTR, 10 times as large as the plug flow reactor, were arranged in series with the existing unit, which unit needs to be arranged first to enhance the production rate.	<b>10</b>	<b>CO2</b>
Q 3	A second order irreversible reaction is carried out in a single CSTR which results in 89% conversion of reactant A. If another identical CSTR is connected in series with the first one determine the percentage increase in conversion of the reactant.	<b>10</b>	<b>CO3</b>
Q 4	Derive the performance equation for recycle reactor.	<b>10</b>	<b>CO4</b>
Q 5	In an isothermal batch reactor 70% of a liquid reactant is converted in 13 min. What space time and space velocity are needed to effect this conversion in a plug flow reactor and in a mixed flow reactor?	<b>10</b>	<b>CO1</b>
Q 6	We plan to replace our present mixed flow reactor with one having double the volume. For the same aqueous feed (10 mol A/liter) and the same feed rate find the new conversion. The reaction kinetics are represented by $A \rightarrow R$ , $-r_A = kC_A^{1.5}$ and present conversion is 70 %.	<b>10</b>	<b>CO2</b>

**SECTION-B (40 Marks)**

Q 7	<p>An aqueous feed of A and B (400 liter/min, 100 mmol A/liter, and 200 mmolB/liter) is to be converted to product in a plug flow reactor. The kinetics of the reaction is represented by <math>A+B \rightarrow R</math>, <math>-r_A= 200 C_A C_B</math> mol/liter.min. Find the volume of reactor needed for 99.9% conversion of A to product.</p>	<b>(20)</b>	<b>CO3 CO4</b>																								
Q 8	<p>We are planning to operate a batch reactor to convert A into R. this is a liquid reaction, the stoichiometry is <math>A \rightarrow R</math>, and the rate of reaction is given in table below. How long must we react each batch for the concentration to drop from <math>C_{A0}= 1.3</math> mol/liter to <math>C_{Af} = 0.3</math> mol/liter?</p> <table border="1" data-bbox="185 575 1338 730"> <tr> <td><math>C_A</math>, mol/liter</td> <td>0.1</td> <td>0.2</td> <td>0.3</td> <td>0.4</td> <td>0.5</td> <td>0.6</td> <td>0.7</td> <td>0.8</td> <td>1.0</td> <td>1.3</td> <td>2.0</td> </tr> <tr> <td><math>-r_A</math>, mol/liter.min</td> <td>0.1</td> <td>0.3</td> <td>0.5</td> <td>0.6</td> <td>0.5</td> <td>0.25</td> <td>0.1</td> <td>0.06</td> <td>0.05</td> <td>0.045</td> <td>0.042</td> </tr> </table>	$C_A$ , mol/liter	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	1.0	1.3	2.0	$-r_A$ , mol/liter.min	0.1	0.3	0.5	0.6	0.5	0.25	0.1	0.06	0.05	0.045	0.042	<b>20</b>	<b>CO5</b>
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$-r_A$ , mol/liter.min	0.1	0.3	0.5	0.6	0.5	0.25	0.1	0.06	0.05	0.045	0.042																