

Name:

Enrolment No:



UNIVERSITY OF PETROLEUM AND ENERGY STUDIES
End Semester Examination, December 2019

Programme Name: M. Tech (Pipeline Engineering)

Semester: 1

Course Name : Numerical Methods in Engineering

Time : 03 hours

Course Code : CHPL7003

Max. Marks: 100

Nos. of page(s) : 03

Instructions:

- i. Use of scientific calculator is allowed for calculations.
- ii. Any pages used for rough work should be attach along with the answer script.

SECTION A

S. No.		Marks	CO
Q 1	Write the general expression for 3 rd order Newton's interpolating polynomial.	4	CO1
Q 2	State the difference between LU decomposition with Gauss elimination method and Crout's decomposition method.	4	CO2
Q 3	State the differences between bracketed and open method for finding the root (s) of an equation.	4	CO3
Q 4	What do you mean by 'stiffness' of ordinary differential equations?	4	CO4
Q 5	What is the difference between Dirichlet and Neumann boundary condition?	4	CO5

SECTION B

Q 6	<p>Use any step size, h, and numerically integrate the following using (i) trapezoidal method, and (ii) Simpson's 1/3 rule to:</p> $\int_0^6 \frac{1}{1+x^2} dx$ <p style="text-align: center;">OR</p> <p>Use 2nd order Lagrange interpolating polynomials to evaluate the value of $f(x)$ at $x = 2$, from the following data given,</p> <table border="1" style="margin-left: auto; margin-right: auto;"><thead><tr><th>X</th><th>$f(x)$</th></tr></thead><tbody><tr><td>1</td><td>0</td></tr><tr><td>4</td><td>0.60206</td></tr><tr><td>6</td><td>0.7782</td></tr></tbody></table>	X	$f(x)$	1	0	4	0.60206	6	0.7782	8	CO1
X	$f(x)$										
1	0										
4	0.60206										
6	0.7782										

Q 7	<p>Use Gauss – Jordan method to solve the following simultaneous linear equations:</p> $3x_1 + 4x_2 + x_3 = 26$ $x_1 + 2x_2 + 6x_3 = 22$ $6x_1 - x_2 - x_3 = 19$ <p>Check your answers by substituting them into the original equations.</p>	8	CO2
Q 8	<p>Determine the real roots of the function, $f(x) = 4x^3 - 6x^2 + 7x - 2.3$, using false position method to locate the roots. Employ an initial guess of, $x_l = 0$, and $x_u = 1$ and make 3 iterations and calculate the approximate error, ε_a for each iteration.</p>	8	CO3
Q 9	<p>Use Euler’s method to numerically solve the following differential equation,</p> $\frac{dy}{dx} = -2x^3 + 12x^2 - 20x + 8.5$ <p>From $x = 0$ to $x = 4$, with a step size (h) of 1. The initial condition at $x = 0$ is $y = 1$. If the true value of the solution at $x = 4$ is 3.0000. Find the true error at $x = 4$.</p>	8	CO4
Q 10	<p>Use the control-volume approach and derive the node equation for node (2, 2) in Fig. 1, and include a heat source at this point. The following constants are given as: $\Delta z = 0.25$ cm, $h = 10$ cm, $k_A = 0.25$ W/cm ·C, and $k_B = 0.45$ W/cm ·C. The heat source comes only from material A at the rate of 6 W/cm³.</p> <div data-bbox="451 1144 1011 1686" data-label="Diagram"> </div> <p>Fig 1: A heated plate with unequal spacing, two materials, and mixed boundary conditions.</p>	8	CO5
SECTION-C			
Q 11	<p>Find the first and second derivative of the following tabulated data at the point, $x = 4$ using (i) forward finite-divided difference, (ii) backward finite-divided difference,</p>	20	CO4

and (iii) centered finite-divided difference. Mention the **error** associated with each of the formula you employ.

x	0	2	4	6	8
$f(x)$	1	7.3891	54.5982	403.4288	2980.9580

Q 12 Use the **Crank- Nicolson** method to solve for the temperature (T) distribution of a long thin rod with a length of 12 cm, at time (t) = 0.2 s. The following values: $k = 0.85 \text{ cm}^2/\text{s}$, and $\rho = 2.7 \text{ g/cm}^3$, step size (Δx) = 3 cm and time step (Δt) = 0.1 s. The equation is given below as:

$$k \frac{\partial^2 T}{\partial x^2} = \frac{\partial T}{\partial t}$$

OR

Use Liebmann's method (Gauss-Seidel) to solve the steady-state heat equation without a heat source over the heated plate in **Fig. 2**. Employ over-relaxation with a value of **1.5** for the weighting factor and iterate to $\epsilon_s = 25\%$. The equation is given below as:

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} = 0$$

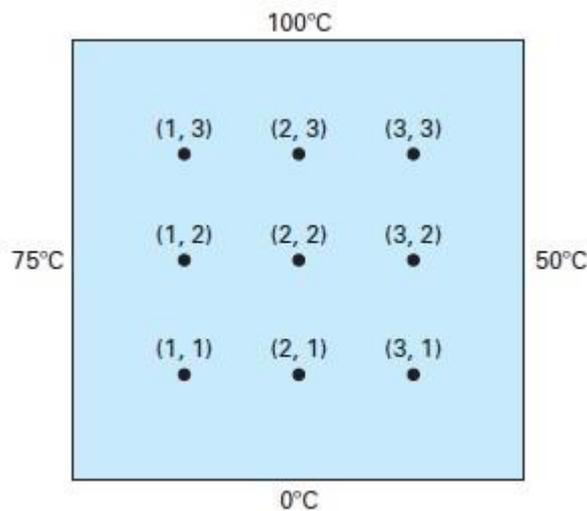


Fig 2: A heated plate where boundary temperatures are held at constant levels.

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CO5