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UNIVERSITY OF PETROLEUM  
AND ENERGY STUDIES



End Semester Examination – May, 2016

Program/course: B.Tech CE + RP/B.Tech APE-Gas  
Subject: Chemical Engineering Thermodynamics-II  
Code : GNEG-423  
No. of page/s: 2

Semester : IV  
Max. Marks : 100  
Duration : 3 Hrs

**PART –A (5 x 4 = 20 marks)**

*(Answer all questions)*

Q. 1	How do you explain the significance of <b>Virial Coefficients</b> ?	CO1
Q. 2	Derive an expression for <b>H<sup>R</sup></b> from <b>Redlich-Kwong EOS</b>	CO2
Q. 3	Explain the <b>graphical method</b> of determination of <b>partial molar properties</b> for a binary solution	CO4
Q. 4	Differentiate between <b>physical &amp; chemical</b> adsorptions	CO5
Q. 5	Differentiate between <b>Dew point &amp; Bubble Point</b> . What is <b>azeotrope</b> ?	CO3

**PART-B (5 x 8 = 40 marks)**

Q. 6	<p>Excess Gibbs free energy of a binary liquid mixture is given by</p> $G^E/RT = x_1x_2 [A + B (x_1-x_2)]$ <p>Show that the activity coefficients are given by,</p> $\ln\gamma_1 = (A + 3B) x_2^2 - 4Bx_2^3$ $\ln\gamma_2 = (A -3B) x_1^2 + 4Bx_1^3,$ <p>where <b>A</b> and <b>B</b> are functions of temperature only and are dimensionless. Obtain Excess Gibbs free energy expression from activity coefficients. Check the activity coefficient expressions satisfy the <b>Gibbs-Duhem</b> equation [8]</p>	CO4
Q. 7	Deduce <b>Gibbs – Duhem</b> equation for a binary system <b>Chemical Potential</b> and also in terms of <b>activity &amp; activity coefficient</b> [4+4]	CO4
Q. 8	Define <b>residual property</b> and obtain the expression for residual properties of pure substances from <b>Virial equation of state</b> . [2+6]	CO2
Q. 9	Reported values for the virial coefficients of <b>Isopropanol</b> vapor at	

	<p><b>200 ° C</b> are,</p> <p><b>B = - 388 cm<sup>3</sup> mol<sup>-1</sup></b>      <b>C = -26,000 cm<sup>6</sup> mol<sup>-2</sup></b></p> <p>Calculate <b>V</b> and <b>Z</b> for Isopropanol vapor at <b>200 ° C</b> and <b>10 bar</b> by</p> <p>(i) The <b>ideal gas</b> equation [2]</p> <p>(ii) Truncated <b>second virial</b> equation [3]</p> <p>(iii) Truncated <b>third virial</b> equation [3]</p>	<b>CO1</b>
Q.10	<p>(a) Define <b>Henry’s Law</b> and mention proper assumptions. [4]</p> <p>(b) Assuming that carbonated water contains only <b>CO<sub>2</sub> &amp; H<sub>2</sub>O</b>, determine the compositions of vapor &amp; liquid phases in a sealed can of “<b>soda</b> “and the pressure exerted on the can at <b>10°C</b>. Henry’s constant for <b>CO<sub>2</sub></b> in water at <b>10°C</b> is about <b>990 bar</b>. <b>P<sub>2sat</sub> = 0.01227 bar @ 283.15 K .</b> [4]</p>	<b>CO3</b>

**PART-C (2 x 20 = marks)**

Q.1 1	<p>Interpret the following models in thermodynamics</p> <p>(i) Van Laar’s model [10]</p> <p>(ii) Margules Two parameter model [10]</p> <p align="center"><b>OR</b></p> <p>The system <b>Acetone (1) / Acetonitrile (2) / Nitromethane (3)</b> at <b>80 ° C</b> and <b>110 kPa</b> has the overall composition <b>z<sub>1</sub> = 0.45, z<sub>2</sub> = 0.35, z<sub>3</sub> = 0.20</b>. Assuming <b>Rauolt’s law</b> is appropriate to this system. Determine <b>L, V, x<sub>i</sub></b> and <b>y<sub>i</sub></b> using <b>flash calculations</b>. [20]</p>	<b>CO3</b>
Q.1 2	<p>At atmospheric pressure <b>Acetone (1)</b> and <b>Chloroform (2)</b> from an <b>azeotrope</b> that boils at <b>64.6 ° C</b> and has a mole fraction of <b>Acetone</b> in the liquid of <b>0.335</b>. The saturation vapour pressure of <b>Acetone</b> and <b>Chloroform</b> at <b>64.6 °C</b> are <b>1.31. &amp; 0.98 atm</b></p> <p>Calculate the activity coefficients using modified <b>Rauolt’s law</b> and <b>Van Laar equation</b> Excess Gibbs free energy and the azeotropic composition, system pressure. [20]</p> <p align="center"><b>OR</b></p> <p>The excess Gibbs free energy of a binary liquid at T &amp; P is given by, <b>G<sup>E</sup>/RT = (-2.6x<sub>1</sub> – 1.8x<sub>2</sub>) x<sub>1</sub> x<sub>2</sub></b></p> <p>(i) Find expression for <b>Y<sub>1</sub></b> and <b>Y<sub>2</sub></b> [10]</p> <p>(ii) Show that the expression satisfies <b>Gibbs-Duhem equation</b> [10]</p>	<b>CO4</b>